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Environment-friendly clay coagulant aid for wastewater treatment

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Abstract

Wastewater management and its environment-friendly applications seem to be very complicated associated with chemical effects due to their dynamic characteristics for developing countries. Most of the world's agencies or countries have been treated wastewater using chemical coagulants which have contributed to other environmental complications. Considering the impacts of chemical coagulation, this study is novel research to identify alternative components that would be applied as a natural coagulant. The present study was conducted using two different regional clays as coagulants which were collected from Portugal and Bangladesh's Patuakhali coastal area. The clay coagulant applications were applied to investigate the removal efficiency of physical properties (turbidity), chemical properties (pH and COD), and heavy metals (Cr, Cd, Ni, and Pb) from wastewater. Comparatively, the highest removal efficiency was examined by the coastal clay of Patuakhali. This soil is also easily available in the local context and can be economically viable.

Keyword Wastewater treatment · Natural coagulant · Turbidity removal · COD reduction

Introduction

Water is an invaluable shared resource with considerable social, cultural, environmental, and economic worth. The rapid growth of the population around the world is associated with using huge quantities of water in different activities including the industrial, agricultural, and household activities (Mohamed et al. 2017). Those activities generate a contaminated wastewater with the chemical and biological residues. Industrial use of water accounts for around one-quarter of worldwide freshwater demand (Judd 1999). About 900 polluting industries in Bangladesh dispose off untreated industrial wastes directly into rivers (DPCD 2003). The wastewaters mainly comprise chemicals like hydrosulfite, sulfide, and sulfur dyes, causing rapid depletion of

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dissolved oxygen, affecting aquatic life adversely (Husain et al. 2013). Therefore, reactive effluents from dying industries create specific chemical hazards and produce several environmental problems (Riera-Torres et al. 2010; Verma et al. 2012). The effluents discharged from textile and dyeing industries may cause alteration of the physical, chemical, and biological properties of the aquatic environment by a continuous change in temperature, odor, noise, turbidity, etc., that is harmful to public health, livestock, wildlife, fish, and another biodiversity (Sultana et al. 2009). Aluminum found in discharged effluents is a major poisoning factor in encephalopathy dialysis and contributes to Alzheimer's disease (Yarahmadi et al. 2009). Polyaluminum chloride (PAC) and alum (AlCl₃) add impurities such as epichloride, which is carcinogenic.

Clay minerals have high cationic exchangeable capacity existing as a natural substance that is used for water treatment and materials absorbance and have other catalysis properties besides low cost and availability (Ingram et al., 2003). It was reported that clay minerals have been used as a coagulant aid removal of toxic compounds, pesticide, herbicide, heavy metals, and color removal (Hascakir et al. 2008). Clay is composed of particles smaller than 2μ , which places them within the limit of the colloidal state (Gillott 1968). Owing to their interesting physicochemical properties (lamellar structure, high surface area)



clay minerals have great potential to fix pollutants, such as heavy metals and organic compounds (Hajjaji et al. 2001), Wu et al. (1999), Laird and Fleming (1999), Viraraghavan and Kapoor (1994), Schutless and Huang (1990) Sharma et al. (1990), and Cadena et al. (1990) have all used clays in batch adsorption experiments for pollutant attenuation in aqueous media. Research findings showed that clays have high potential in water and wastewater treatment. Clay minerals have a high cationic exchangeable capacity that exists as a natural substance used for water treatment and materials absorbance. They also have other catalytic properties besides low cost and availability (Ingram et al. 2003). It was reported that clay minerals had been used as a coagulant aid for removal of toxic compounds, pesticide, herbicide, heavy metals, and color (Hascakir et al. 2008). The use of clay mineral has undoubtedly become more popular and widely used as an adsorbent and ion exchange for water and wastewater treatment applications specially for removing heavy metals, organic pollutants, and nutrients (Abdelaal 2004). In Bangladesh, treating industrial wastewater is a great challenge due to the high cost of chemical coagulants (Awad et al. 2013) and their side effects. Therefore, the current study deals with natural clay coagulants' technical feasibility for the treatment and improvement of wastewater before the final disposal into the environment. The researchers' main objectives are to develop clay-based coagulant aid for effluent treatment plant (ETP) and characterize the developed coagulants.

Materials and methods

Sampling stations

Clay samples for coagulants were collected from Patuakhali, a coastal area of Bangladesh (Fig. 1a, b) and from Portugal (Fig. 1c). Wastewater samples were collected from different textile industries in Gazipur, Bangladesh.

Sample collection and preparation

Wastewater sample collection

Wastewater samples were collected from five textile industries of Gazipur district, Bangladesh, following the sampling techniques as outlined by APHA (1995). The effluent samples were collected in 500-mL plastic bottles from every selected industry to analyze pH, turbidity, COD, and heavy metals. Before sample collection, all the bottles were washed with tap water followed by distilled water. Sampling followed the sampling techniques as outlined by APHA (1995).



Soil sample collection

Two soil samples were collected from two stations of Hazipara under Kolapara thana in Patuakhali, Bangladesh, and one from Portugal. Samples were collected in zip lock bags. After collection, the samples were carefully carried to the laboratory and from the samples, the gravels, pebbles, plant roots; leaves, etc., were separated. The samples were dried in air for 15 days by spreading on a clean piece of polythene bags. The dried samples were mortared to a fine powder and passed through a plastic sieve of 0.3 mm diameter and preserved in aluminum foil paper for laboratory analysis.

Optimization of coagulant dosage

In the initial stage of the study, the efficiency of the coagulants was tested in terms of the reduction of turbidity. The results from this stage of study encouraged to proceed further to the second stage, with the coagulant dosage optimized at 1, 1.5, 2, and 2.5 g/L. American Water Works Agency (AWWA) 5220D (Closed Reflux, Colorimetric Method) was used for dosage optimization. 1.5 g/L dose was selected for Patuakhali soil, and 2.5 g/L dose was selected for soil Portugal.

Optimization of pH

The optimum value of pH depends essentially on the properties of the water treated, type of coagulant used and its concentration. Usually, after the addition of different coagulants, the pH of the treated wastewater decreased from 5.81 to 7.03 (Sanchez et al. 2012). Following the determination of the optimum dosage of the coagulants, pH test was carried out to determine the optimum range of the pH value, which gives the highest turbidity removal. Hydrochloric acid (HCl) 0.1 M and sodium hydroxide (NaOH) 0.1 M were used for adjusting the pH at the desired levels (2,4,6,8).

Optimization of temperature and contact time

The temperature for the thermo-reactor was optimized at 150°C, and the contact time was 1 h and 45 min.

Volume optimization

According to AWWA 5220D method, 212.5 mg potassium hydrogen phthalate with 500 ml DI water (500 ppm COD) was taken in a volumetric flask. From this solution 50 ml, 100 ml, 150 ml, and 200 ml were taken in four conical flasks and soil samples were added in each. Then, these flasks were placed on the shaker and filtered by syringe filter paper. After that 2.5 ml soil samples, 1.5 ml digestion solution and 3.5 ml sulfuric acid solution were received in vials and placed those in a





Fig. 1 a Map of wastewater collection area. b Map of soil sample collection area of Patuakhali, Bangladesh. c Map of soil sample collection area, Portugal





Fig. 1 (continued)

thermo-reactor for 2 h at 150°C. Afterward, 200 ml volume of waste water was selected for 1.5gm soil and 50 ml was selected for 2.5gm soil.

Removal efficiency

The removal efficiency of turbidity, COD, and heavy metals was calculated according to the following formula:

Removal efficiency (%) =
$$\frac{(C_i - C_f)}{C_i} \times 100$$
 (1)

where C_i is the Initial concentration of the parameter and C_f is the final concentration of the parameter.

Statistical analysis

Data were analyzed using software MS Excel for graphical presentation. Values were expressed as mean \pm SEM (standard error of mean). Correlation among the parameters has been done according to the Pearson correlation process in Statistical Package for Social Science (IBM SPSS Statistics 20.0).

Results and discussion

Physicochemical parameters of the effluents

Physicochemical properties of wastewater were determined before and after treatment with clay coagulants enable to predict the removal efficiency of clay coagulants.



Watercolor and odor

The initial color of wastewater for all samples was dark violet to black. After the treatment, water from every sample was found nearly colorless and transparent. The odor of wastewater in all samples was observed pungent to high pungent. After treatment, the samples became odorless. The odor of freshwater samples was nearly odorless.

Turbidity

The primary mean values of turbidity were 50.14 NTU, 59.66 NTU, 252 NTU, 70.66 NTU, and 119.33 NTU found



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Fig. 2 Turbidity of water before and after treatment

Table 1Average value andremoval efficiency (%) of claycoagulant

r al allicici s		IIIIIai	FK5 01	FK5 02	гкэ
Turbidity	Average value	110.35	31.51	39.98	7.04
	Removal efficiency (%)		77.44	63.77	93.62
рН	Average value	9.487	8.34	8.37	7.82
	Removal efficiency (%)		12.02	11.71	17.52
COD	Average Value	745.53	417.56	397.18	469.14
	Removal efficiency (%)		43.99	46.72	37.07
Chromium (Cr)	Average value	93.14	13.68	8.88	9.84
	Removal efficiency (%)		85.30	90.49	89.42
Cadmium (Cd)	Average value	1.78	1.04	1.55	1.61
	Removal efficiency (%)		41.59	12.59	9.21
Lead (Pb)	Average value	208.52	BDL	1.09	8.69
	Removal efficiency (%)		N/A	99.47	95.82
Nickel (Ni)	Average value	67.98	38.85	43.89	66.72
	Removal efficiency (%)		42.85	35.43	1.85

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in stations 1,2,3,4, and 5, respectively (Fig. 2). When turbid samples were treated by clay from Patuakhali Clay sample-1(PKS-1), then the turbidity of wastewater from the station-1,2,3,4, and 5 decreased to 18.92 NTU, 58 NTU, 47.35 NTU, 25.62 NTU, and 7.70 NTU, respectively. After adding clay soil from Patuakhali clay sample-2(PKS-2), the turbidity decreased gradually to 45.86 NTU, 57 NTU, 73.33 NTU, 19.38 NTU, and 4.33NTU in station 1, 2, 3, 4, and 5, respectively. After adding clay from the Portugal clay sample (PRS), the turbidity decreased correlatively to 3.89 NTU, 15.43 NTU, 2.84 NTU, 9.27 NTU, and 3.77NTU in the water samples of station-1,2,3,4, and 5, respectively. It is revealed that the addition of clay coagulants can result in the reduction of turbidity in wastewater.

Turbidity removal efficiency obtained from PKS 01, PKS 02, and PRS was 77.44%, 63.77%, and 93.62%, respectively, to attain final turbidity 31.51 NTU, 39.98 NTU, and 7.04 NTU, respectively (Table 1). The highest efficiency (93.62%) was found for the Portugal clay sample (PRS). According to Awad et al. (2013), the removal efficiency for polyaluminum chloride (PAC) and its combined use with Shendi and Singa for turbidity was 96.2%, 94.8%, and 95.7%, which almost coincided with PRS of the present study. Kuipa et al. (2015) found Katonda clay in combination with alum for the treatment of surface water for drinking purposes with optimum turbidity removal of 89.9% at a dosage rate of 30 mg/L (30 mg/L Alum, 30 mg/L Clay). Saritha et al. (2017) showed that the removal of turbidity was up to 99% by both alum and chitin at lower doses of coagulant, i.e., 0.1-0.3 g/L, whereas sago has shown a reduction of 70-100% at doses of 0.1 and 0.2 g/L. However, using only natural clay coagulant, the present study gained the removal efficiency of 77.44% for PKS-1, 63.77% for PKS-2 at doses of 1.5 g/L, and 93.62% for PRS at doses of 2.5 g/L.

DVC 01

DVC 02

DDC





Fig. 3 pH of wastewater before and after treatment



Fig. 4 COD of wastewater before and after treatment

pН

The initial mean pH in station-1,2,3,4, and 5 was 9.36, 11.15, 8.61,10.46, and 7.85, respectively (Fig. 3). After treating with the clay coagulant from PKS-1, the pH decreased to 7.84 (station-1), 8.80 (station-2), 3 7.78 (station-4), and 9.8 (station-5). When clay coagulant of PKS-2 was used for treatment, the pH was reduced to 7.91, 8.77,7.82, 9.89, and 7.48 in the station 1,2,3,4, and 5, respectively, while using clay of PRS, the pH became 7.62, 7.54, 7.45, 9.68, and 6.81 in station-1,2,3,4, and 5, respectively.

However, the pH of the effluents was always higher when those were discharged from the industry. It might be due to the presence of alkaline wastes in industrial effluents. Here it is found that in all stations the pH has been decreased after adding clay soils as coagulants. Roy et al. (2010) used *Saccostrea cucullata* and *Pistia stratiotes* as a natural coagulant which reduced pH 22.50% and 22.18%, respectively. In the present study for use of soil coagulant the reduction efficiency of pH was 12.02%, 11.71%, and 17.52% from PKS 1, PKS 2, and PRS to attain final pH 8.34, 8.37, and 7.82 (Table 1), respectively, where the highest efficiency was found for PRS. The national standard of pH for the industrial units in Bangladesh is 6–9 (DoE 2008). The achieved result for pH after treatment remains within the standard.

Chemical oxygen demand (COD)

At the preliminary stage, the COD of the raw samples was 609.85 ppm, 736.23 ppm, 611.88 ppm, 1183.38 ppm, and 586.49 ppm found in station 1,2,3,4, and 5, respectively (Fig. 4). After treating with clay from PKS-1, the COD significantly reduced to 376.30 ppm, 616.53 ppm, 139.40 ppm, 746 ppm, and 209.57 ppm for station 1,2,3,4, and 5, respectively. Treating by clay from PKS-2, the COD decreased to



225.35 ppm, 578.94 ppm, 229.62 ppm, 724.53 ppm, and 227.45 ppm that are place d in station 1,2,3,4, and 5 sequentially. After using clay from PRS, the concentration of COD values in station 1,2,3,4, and 5 is 422.18 ppm, 536.07 ppm, 269.66 ppm, 777.06 ppm, and 340.74 ppm, respectively. The standard value of suggested effluent discharge is 200 ppm (DoE 2008). The yield value after treatment was almost to the standard level. Though all the treated wastewater was not within the standard limit of DoE(2008), still these were lower than the raw wastewater. Based on Pearson correlation analysis between PKS-1 dosed wastewater and PKS-1 soil properties, a strong positive correlation was found between COD and pH (r = 0.93, p < 0.05) and COD and Fe (r = 0.93, p < 0.05) (Table 2). Similarly, a correlation was found between PKS-2 dosed wastewater and PKS-2 soil properties, as well as PRS, dosed wastewater, and PRS soil properties; a strong positive correlation was found between COD and pH (r=0.96, p<0.01) (Table 3) and (r=0.88, p<0.01) (Table 4), respectively.

Shah et al. (2015) found in a treatment that coagulant of FeSO₄ lime influenced 32% reduction of COD, whereas the removal efficiencies obtained from the present study are more than that of the findings of Husain et al. (2013), who showed that the physicochemical method of coagulation and flocculation using alum with clay produced 92% COD removal where using soil without any chemical in this study has achieved 43.99%, 46.72%, and 37.07% COD removal efficiency for PKS 01, PKS 02, and PRS, respectively (Table 1). Though Awad et al. (2013) found better removal efficiency for polyaluminum chloride (PAC) and its combined use with Shendi and Singa for COD, which were 70.7%, 63.2%, and 61.1%. It is revealed that the quality of treated effluent using PKS-1 and PKS-2 clay coagulants is Table 2Correlation analysis for
clay coagulant PKS-1

	pН	Turbidity	COD	Cd	Cr	Ni	Pb	Al	Fe	Cl-	SO_4^{2-}
рН	1										
Turbidity	0.26	1									
COD	0.93*	0.20	1								
Cd	0.85	-0.15	0.70	1							
Cr	-0.01	0.05	0.33	-0.33	1						
Ni	0.88*	-0.12	0.74	0.99**	-0.30	1					
Pb	.b	.b	.b	.b	.b	.b	.b				
Al	.0.56	0.70	0.59	0.19	0.38	0.22	.b	1			
Fe	0.79	-0.04	0.93*	0.65	0.49	0.67	.b	0.54	1		
Cl-	0.51	0.43	0.52	0.22	0.04	0.27	.b	0.09	0.23	1	
SO_4^{2-}	0.91*	0.58	0.77	0.69	-0.17	0.72	.b	0.63	0.53	0.61	1

*Correlation is significant at 0.05 level (2-tailed)

**Correlation is significant at 0.01 level (2-tailed)

^bCannot be computed because at least one of the variables is constant

Table 3Correlation analysis forclay coagulant PKS-2

	pН	Turbidity	COD	Cd	Cr	Ni	Pb	Al	Fe	Cl-	SO42-
pН	1										
Turbidity	-0.12	1									
COD	0.96**	-0.15	1								
Cd	0.87	-0.41	0.76	1							
Cr	0.33	-0.14	0.33	0.10	1						
Ni	0.89*	-0.37	0.80	0.99**	0.11	1					
Pb	0.22	0.34	0.42	-0.25	0.36	-0.19	1				
Al	-0.10	-0.20	0.07	-0.39	0.67	037	0.67	1			
Fe	-0.71	0.63	-0.74	-0.84	0.09	-0.84	0.07	0.17	1		
Cl-	0.72	-0.52	0.74	0.62	0.78	0.63	0.25	0.45	-0.55	1	
SO_4^{2-}	0.54	0.12	0.35	0.72	-0.36	0.72	-0.48	-0.88*	-0.43	-0.02	1

*Correlation is significant at 0.05 level (2-tailed)

**Correlation is significant at 0.01 level (2-tailed)

Table 4Correlation analysis for
clay coagulant PRS

	pН	Turbidity	COD	Cd	Cr	Ni	Pb	Al	Fe	Cl-	SO ₄ ²⁻
рН	1										
Turbidity	0.31	1									
COD	0.88*	0.62	1								
Cd	0.95*	0.23	0.86	1							
Cr	-0.10	0.73	0.32	-0.18	1						
Ni	0.94*	0.57	0.98**	0.91*	0.18	1					
Pb	0.95*	0.23	0.86	0.98**	-0.18	0.91*	1				
Al	-0.15	-0.68	-0.52	-0.30	-0.53	-0.43	-0.30	1			
Fe	0.76	-0.64	-0.74	-0.72	0.01	-0.80	-0.72	0.41	1		
Cl-	0.32	-0.42	-0.10	0.15	-0.63	0.02	0.15	0.84	-0.13	1	
SO_4^{2-}	0.50	-0.20	0.26	0.66	-0.71	0.36	0.66	-0.15	-0.52	0.19	1

*Correlation is significant at 0.05 level (2-tailed)

**Correlation is significant at 0.01 level (2-tailed)



quite satisfactory. These results indicate that clay coagulants used in the present study would be efficient for the removal of COD from such wastewater.

Chromium (Cr)

The optimum concentration of chromium (Cr) for GFAAS machine ranges from 5 to 100 ppb. The elementary concentration of Cr in effluents for station-1 was 112.98 ppb, for station-2 it was 95.62 ppb, for station-3 it was 39.122 ppb, for station-4 was 25.923 ppb, and for station-5 it was 192.09 ppb (Fig. 5). But after treating with clay from PKS-1, the concentration of Cr decreased to 25.70 ppb, 25.32 ppb, 6.77 ppb, and 10.62 ppb for station-1,2,4, and 5, respectively, and in treatment by clay soil of PKS-2, the concentration of Cr reduced for station-1 (15.63 ppb) for station-2, 4, and 5 (12.83 ppb, 10.06 ppb, and 5.76 ppb, respectively), whereas after treatment by PRS clay sample, the concentration of Cr reduced for station-1 (12.6 ppb), station-2, 4, and 5 (20.01 ppb, 7.48 ppb, and 9.13 ppb, respectively). Mahmood et al. (2005) used Eichhornia crassipies for wastewater treatment and recorded 78.30% to 94.78% reduction where the present study provides 85.3%, 90.49%, and 89.42% removal for PKS 1, PKS 2 and PRS (Table 1). According to DoE (2008), the discharge limit of total Cr (as Cr molecule) in a classified textile industry is 2 mg/L.

Cadmium (Cd)

The optimum concentration of cadmium (Cd) for GFAAS ranges from 0.5 to 10 ppb. The initial content of Cd in the effluent for station-1, 2, 3, and 5 is under outlier and for station-4 it is 8.896 ppb. After adding clay from PKS-1 and

PKS-2 and PRS, Cd's concentration for station-1, 2, 3, and 5 is under outlier and for station-4 it was 5.19 ppb, 7.77 ppb, and 8.07 ppb, respectively (Fig. 6). The removal efficiencies for PKS-1, PKS-2, and PRS were found 41.59%, 12.59%, and 9.21%, respectively (Table 1). The efficiency was high in PKS-1. Based on correlation analysis between PRS dosed wastewater and PRS soil properties, strong positive correlation was found between Cd and pH (r=0.95, p<0.01) (Table 4).

Lead (Pb)

The optimum concentration of lead (Pb) for GFAAS ranged from 5 to 100 ppb. The primary concentration of lead (Pb) for station-1, 2, 3, 4, and 5 is 423.07 ppb, 57.13 ppb, 167.25 ppb, 130.33 ppb, and 264.83 ppb gradually (Fig. 7). After using clay from PKS-1, the concentration of lead (Pb) is under outlier for all the wastewater samples and using clay from PKS-2 and PRS, the concentrations of lead (Pb) for wastewater sample station-1, 2, 3, and 5 are below detection and for station-4, it is 5.49 ppb and 43.49 ppb, respectively. The removal efficiency for PKS-1 is not detected, but for PKS-2 and PRS is 99.47% and 95.82% (Table 1). Based on correlation analysis between PRS dosed wastewater and PRS soil properties, strong positive correlation was found between Pb and pH (r=0.95, p<0.01), Pb and Cd (r=0.98, p < 0.01), and Pb and Ni (r = 0.91, p < 0.01) (Table 4). In this aspect, the efficiency is high in PKS-2. Tiruneh et al. (2018) observed high percentage removal of lead which was ranging from 98.84 to 99.69% by using aluminum sulfate with clay.









Fig. 7 Pb concentration before and after treatment



Fig. 8 Ni concentration before and after treatment

Nickel (Ni)

The optimum concentration of nickel (Ni) for GFAAS ranges from 5 to 100 ppb. The initial concentration of Ni in station-1,2,3, and 4 is 43.08 ppb, 33.19 ppb, 54.07 ppb, and 209.58 ppb (Fig. 8). Using clay soil from PKS-1, the concentration of nickel (Ni) for water sample station-1, 3, and 5 is not detected and for station-2 and 4, these are 10.34 ppb and 183.91 ppm, respectively, whereas using soil from PKS-2, the concentration of nickel (Ni) for station-1 and 5 is below detection and for station-2,3, and 4, these are 13.64 ppb and 5.99 ppb and 199.82 ppb, respectively. Adding clay soil from PRS, the concentration of nickel (Ni) for station-3 and 5 is an outlier and for station-1, 2, and 4, those are 38.96 ppb, 85.33 ppb, and 209.33 ppb gradually. The standard limit of Ni in surface water of Bangladesh is 1.0 ppm (DoE 2008).

Based on Pearson correlation analysis between PKS 01 dosed wastewater and PKS-1 soil, a strong positive correlation was found between Ni and pH (r=0.88, p<0.05) and Ni and Cd (r=0.99, p<0.01) (Table 2), and between PKS-2 dosed wastewater and PKS-2 soil properties a strong positive correlation was found between Ni and Cd (r=0.99, p<0.01) (Table 3) and Ni and pH (r=0.89, p<0.05), and between PRS dosed wastewater and PRS soil properties a strong positive correlation was found between Ni and pH (r=0.99, p<0.01), (Table 3) and Ni and pH (r=0.89, p<0.05), and between PRS dosed wastewater and PRS soil properties a strong positive correlation was found between Ni and pH (r=0.94, p<0.01),Ni and COD (r=0.98, p<0.01), and Ni and Cd (r=0.91, p<0.01) (Table 4).

Esmaeili et al. (2019) observed the removal efficiency of Ni by bentonite at dose 60 g/l was 99.9%. The removal efficiencies for PKS-1, PKS-2, and PRS were 42.85%, 35.43%, and 1.85%, respectively (Table 1). The efficiency was high (42.85%) in PKS-1 and very poor in PRS.

It is revealed from experimental analysis in some cases, physicochemical parameters (such as color, odor, pH, turbidity, COD) and heavy metals (like Cr, Cd, Pb, and Ni) of industrial wastewater were higher than that of the recommended value set by DoE (2008) and ECR (1997).

Results for the treatment with clay coagulants show significant efficiency in most of the cases. In this case, more pollutant removal efficiency was found for local clay (PKS1, PKS2). However, some previous researchers found better efficiency using different coagulants for pollutant removal.

Conclusion

The study revealed the potentiality and effectiveness of natural clay as a coagulant in the removal of pollutants from wastewater. Clay coagulants have been shown the ability in the removal of pollutants for the gainful application. In this study, the industrial wastewater was treated with clay collected from Portugal and Patuakhali coastal area of Bangladesh to investigate its efficiency in reducing pH, COD, and heavy metals including Cd, Cr, Ni, and Pb. The removal efficiencies for turbidity, pH, COD, Cd, Cr, Ni, and Pb are 77.44%, 12.02%, 43.99%, 41.59%, 85.30%, and 42.85% for Patuakhali clay-1; 63.77%, 11.71%, 46.72%, 12.59%,90.49%, 35.43%, and 99.47% for Patuakhali clay-2; and 93.62%, 17.52%, 37.07%, 9.21%, 89.42%, 1.85%, and 95.82% for Portugal clay, respectively.

The technology of using soil for the treatment of industrial wastewater is an alternative method to the conventional methods available. It is more cost-effective for us. The result is satisfactory for our native local soil than foreign soil, and moreover, local soil is available and easy to collect. Furthermore, research should be performed to determine the removal efficiency of biological contaminants and other heavy metals of wastewater utilizing soil. Beside these, a wide variety of soils need to be examined to find out prominent coagulants for wastewater treatment.



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Declarations

Conflict of interest There is no conflict of interest regarding this manuscript.

Ethical approval Authors firmly abide by all ethical norms and follow the guidelines set by COPE.

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